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MULTIMEDIA UNIVERSITY

FINAL EXAMINATION

TRIMESTER 2, 2022/2023 (TERM ID 2220)

EME3026 – FLUID DYNAMICS
(ME)

4 JULY 2023
9:00 – 11:00 a.m.
(2 Hours)

INSTRUCTIONS TO STUDENTS

1. This exam paper consists of only nine printed pages, including this cover page.
2. Answer all questions.
3. Write all your answers in the answer booklet provided.

Question 1

a). If the stream function for a flow is $\psi = (8x + 6y) \text{ m}^2/\text{s}$, where x and y are in meters, determine the potential function, and the magnitude of the velocity of a fluid particle at point $(2 \text{ m}, -1.5 \text{ m})$. [13 marks]

b). The velocity within the eye of a tornado is defined by

$$v_r = 0, v_\theta = (0.4r) \text{ m/s},$$

where r is in meters. See Fig. 1b. Determine the circulation at $r = 100 \text{ m}$ and at $r = 200 \text{ m}$. [12 marks]

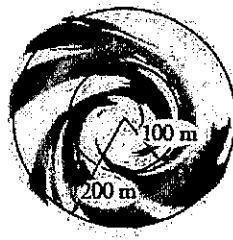


Figure 1b

Question 2

a). A fire hydrant supplies water under a pressure of 250 kPa. See Fig. 2a. If a 100-mm diameter hose is connected to it at A and the hose extends 40m to the fire truck inlet at B , determine the pressure of the water as it arrives at B . The friction loss is 1.2 m for every 10m of hose. The inlet at B is 0.5 m higher than the hydrant outlet. [13 marks]

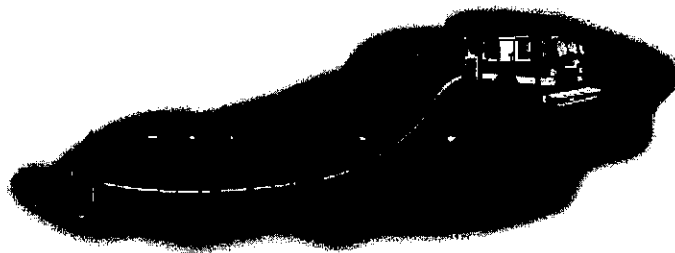


Figure 2a

b). Particles travel within a flow field defined by $\mathbf{V} = 2y^2\mathbf{i} + 4y\mathbf{j} \text{ m/s}$, where x and y are in meters. Determine the equation of the streamline passing through point $(1 \text{ m}, 2 \text{ m})$, and find the velocity of a particle located at this point. Draw this streamline. [12 marks]

Continued . . .

Question 3

a). The 100-mm-diameter shaft is supported by an oil lubricated bearing. See Fig. 2a. If the gap within the bearing is 2 mm, determine the torque T that must be applied to the shaft, so that it rotates at a constant rate of 180 rev/min. Assume no oil leaks out, and the flow behavior is similar to that which occurs between parallel plates, since the gap size is very much smaller than the radius of the shaft. Take $\rho_o = 840 \text{ kg/m}^3$ and $\mu_o = 0.22 \text{ N s/m}^2$. [13 marks]

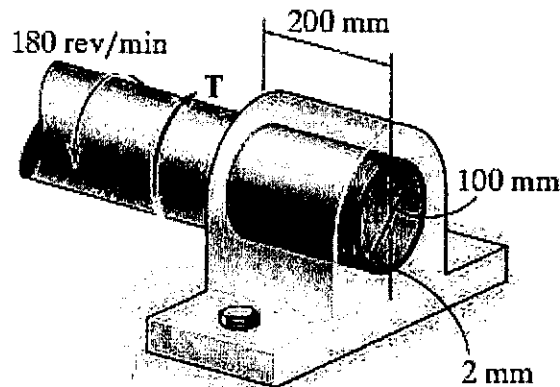


Figure 2a

b). SAE 10W-30 oil flows through the 125-mm-diameter pipe with an average velocity of 2 m/s. See Fig. 2b. Determine the drop in pressure caused by viscous friction over the 10-m-long section. Take $\rho_o = 920 \text{ kg/m}^3$ and $\mu_o = 0.2 \text{ N s/m}^2$. [12 marks]

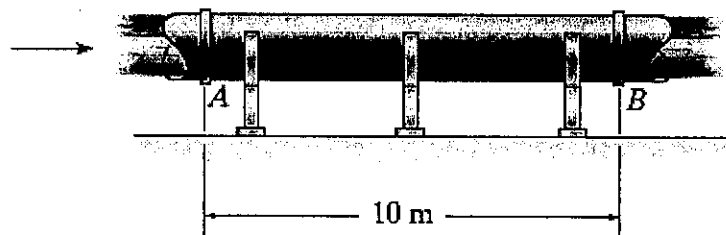


Figure 2b

Continued . . .

Question 4

- a). The Mach number of the air flow out the nozzle at B is $M = 0.4$. See Fig. 4a. If the air has a temperature of 8°C and absolute pressure of 20 kPa, determine the absolute pressure and temperature of the air within the large reservoir at A. [13 marks]

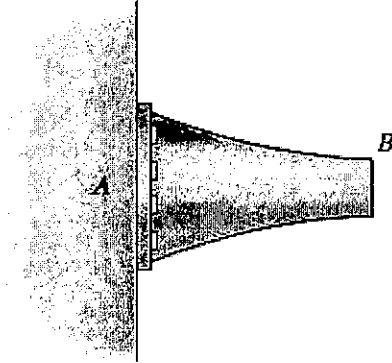


Figure 4a

- b). What is water hammer? State five effects of water hammer. [12 marks]

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Appendices

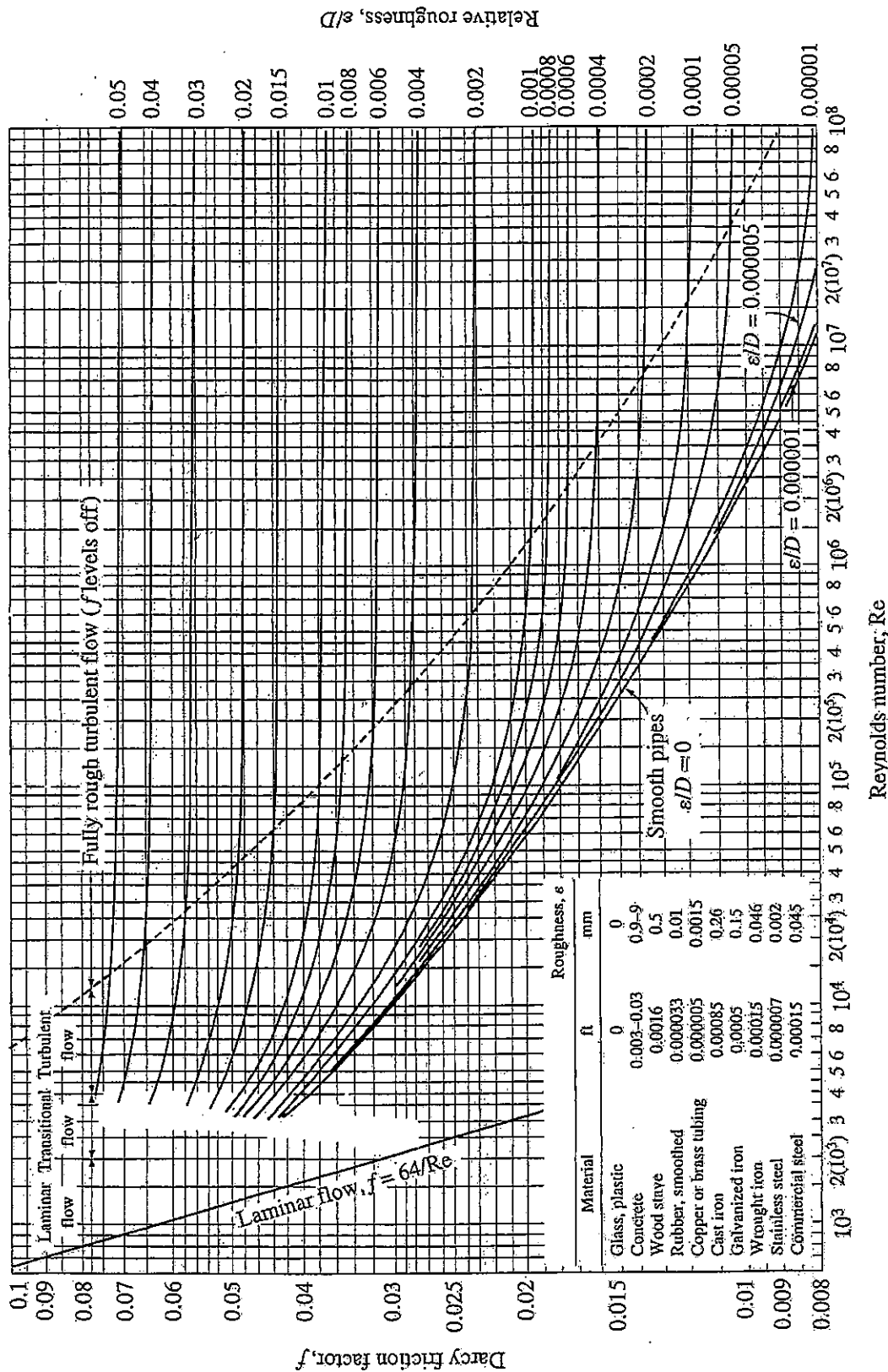


FIGURE A-12

The Moody chart for the friction factor for fully developed flow in circular pipes for use in the head loss relation $h_L = f \frac{L}{D} \frac{V^2}{2g}$. Friction factors in the turbulent flow are evaluated from the Colebrook equation $\frac{1}{\sqrt{f}} = -2 \log_{10} \left(\frac{\epsilon/D}{3.7} + \frac{2.51}{Re \sqrt{f}} \right)$.

Continued...

$$Ma^* = Ma \sqrt{\frac{k+1}{2+(k-1)Ma^2}}$$

$$\frac{A}{A^*} = \frac{1}{Ma} \left[\left(\frac{2}{k+1} \right) \left(1 + \frac{k-1}{2} Ma^2 \right) \right]^{0.5(k+1)/(k-1)}$$

$$\frac{P}{P_0} = \left(1 + \frac{k-1}{2} Ma^2 \right)^{-k/(k-1)}$$

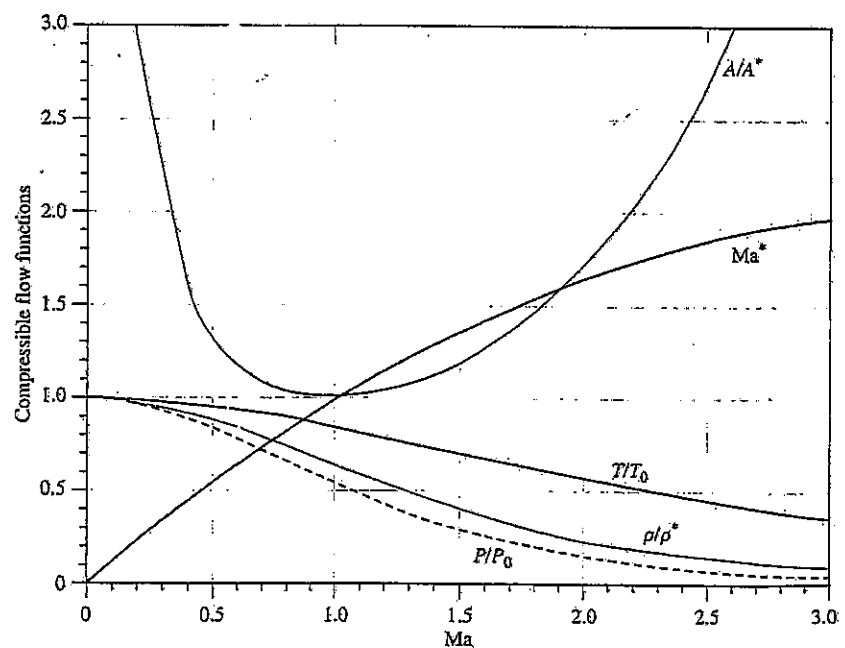
$$\frac{\rho}{\rho_0} = \left(1 + \frac{k-1}{2} Ma^2 \right)^{-1/(k-1)}$$

$$\frac{T}{T_0} = \left(1 + \frac{k-1}{2} Ma^2 \right)^{-1}$$

TABLE A-13

One-dimensional isentropic compressible flow functions for an ideal gas with $k = 1.4$

Ma	Ma*	A/A*	P/P ₀	ρ/ρ ₀	T/T ₀
0	0	∞	1.0000	1.0000	1.0000
0.1	0.1094	5.8218	0.9930	0.9950	0.9980
0.2	0.2182	2.9635	0.9725	0.9803	0.9921
0.3	0.3257	2.0351	0.9395	0.9564	0.9823
0.4	0.4313	1.5901	0.8956	0.9243	0.9690
0.5	0.5345	1.3398	0.8430	0.8852	0.9524
0.6	0.6348	1.1882	0.7840	0.8405	0.9328
0.7	0.7318	1.0944	0.7209	0.7916	0.9107
0.8	0.8251	1.0382	0.6560	0.7400	0.8865
0.9	0.9146	1.0089	0.5913	0.6870	0.8606
1.0	1.0000	1.0000	0.5283	0.6339	0.8333
1.2	1.1583	1.0304	0.4124	0.5311	0.7764
1.4	1.2999	1.1149	0.3142	0.4374	0.7184
1.6	1.4254	1.2502	0.2353	0.3557	0.6614
1.8	1.5360	1.4390	0.1740	0.2868	0.6068
2.0	1.6330	1.6875	0.1278	0.2300	0.5556
2.2	1.7179	2.0050	0.0935	0.1841	0.5081
2.4	1.7922	2.4031	0.0684	0.1472	0.4647
2.6	1.8571	2.8960	0.0501	0.1179	0.4252
2.8	1.9140	3.5001	0.0368	0.0946	0.3894
3.0	1.9640	4.2346	0.0272	0.0760	0.3571
5.0	2.2361	25.000	0.0019	0.0113	0.1667
∞	2.2495	∞	0	0	0



Continued ...

$$T_{01} = T_{02}$$

$$Ma_2 = \sqrt{\frac{(k-1)Ma_1^2 + 2}{2kMa_1^2 - k + 1}}$$

$$\frac{P_2}{P_1} = \frac{1 + kMa_1^2}{1 + kMa_2^2} = \frac{2kMa_1^2 - k + 1}{k + 1}$$

$$\frac{\rho_2}{\rho_1} = \frac{P_2/P_1}{T_2/T_1} = \frac{(k+1)Ma_1^2}{2 + (k-1)Ma_1^2} = \frac{V_1}{V_2}$$

$$\frac{T_2}{T_1} = \frac{2 + Ma_1^2(k-1)}{2 + Ma_2^2(k-1)}$$

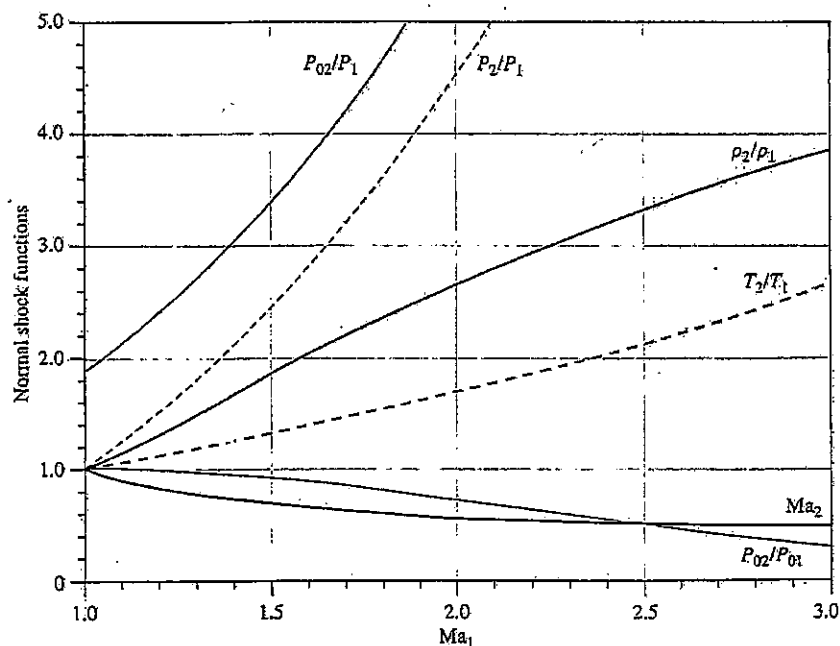
$$\frac{P_{02}}{P_{01}} = \frac{Ma_1 [1 + Ma_2^2(k-1)/2]^{(k+1)/(2(k-1))}}{Ma_2 [1 + Ma_1^2(k-1)/2]^{(k+1)/(2(k-1))}}$$

$$\frac{P_{02}}{P_1} = \frac{(1 + kMa_1^2)[1 + Ma_2^2(k-1)/2]^{k/(k-1)}}{1 + kMa_2^2}$$

TABLE A-14

One-dimensional normal shock functions for an ideal gas with $k = 1.4$

Ma_1	Ma_2	P_2/P_1	ρ_2/ρ_1	T_2/T_1	P_{02}/P_{01}	P_{02}/P_1
1.0	1.0000	1.0000	1.0000	1.0000	1.0000	1.8929
1.1	0.9118	1.2450	1.1691	1.0649	0.9989	2.1328
1.2	0.8422	1.5133	1.3416	1.1280	0.9928	2.4075
1.3	0.7860	1.8050	1.5157	1.1909	0.9794	2.7136
1.4	0.7397	2.1200	1.6897	1.2547	0.9582	3.0492
1.5	0.7011	2.4583	1.8621	1.3202	0.9298	3.4133
1.6	0.6684	2.8200	2.0317	1.3880	0.8952	3.8050
1.7	0.6405	3.2050	2.1977	1.4583	0.8557	4.2238
1.8	0.6165	3.6133	2.3592	1.5316	0.8127	4.6695
1.9	0.5956	4.0450	2.5157	1.6079	0.7674	5.1418
2.0	0.5774	4.5000	2.6667	1.6875	0.7209	5.6404
2.1	0.5613	4.9783	2.8119	1.7705	0.6742	6.1654
2.2	0.5471	5.4800	2.9512	1.8569	0.6281	6.7165
2.3	0.5344	6.0050	3.0845	1.9468	0.5833	7.2937
2.4	0.5231	6.5533	3.2119	2.0403	0.5401	7.8969
2.5	0.5130	7.1250	3.3333	2.1375	0.4990	8.5261
2.6	0.5039	7.7200	3.4490	2.2383	0.4601	9.1813
2.7	0.4956	8.3383	3.5590	2.3429	0.4236	9.8624
2.8	0.4882	8.9800	3.6636	2.4512	0.3895	10.5694
2.9	0.4814	9.6450	3.7629	2.5632	0.3577	11.3022
3.0	0.4752	10.3333	3.8571	2.6790	0.3283	12.0610
4.0	0.4350	18.5000	4.5714	4.0469	0.1388	21.0681
5.0	0.4152	29.0000	5.0000	5.8000	0.0617	32.6335
∞	0.3780	∞	6.0000	∞	0	∞



Continued ...

$$\frac{T_0}{T_0^*} = \frac{(k+1)Ma^2[2 + (k-1)Ma^2]}{(1 + kMa^2)^2}$$

$$\frac{P_0}{P_0^*} = \frac{k+1}{1 + kMa^2} \left(\frac{2 + (k-1)Ma^2}{k+1} \right)^{k/(k-1)}$$

$$\frac{T}{T^*} = \left(\frac{Ma(1+k)}{1 + kMa^2} \right)^2$$

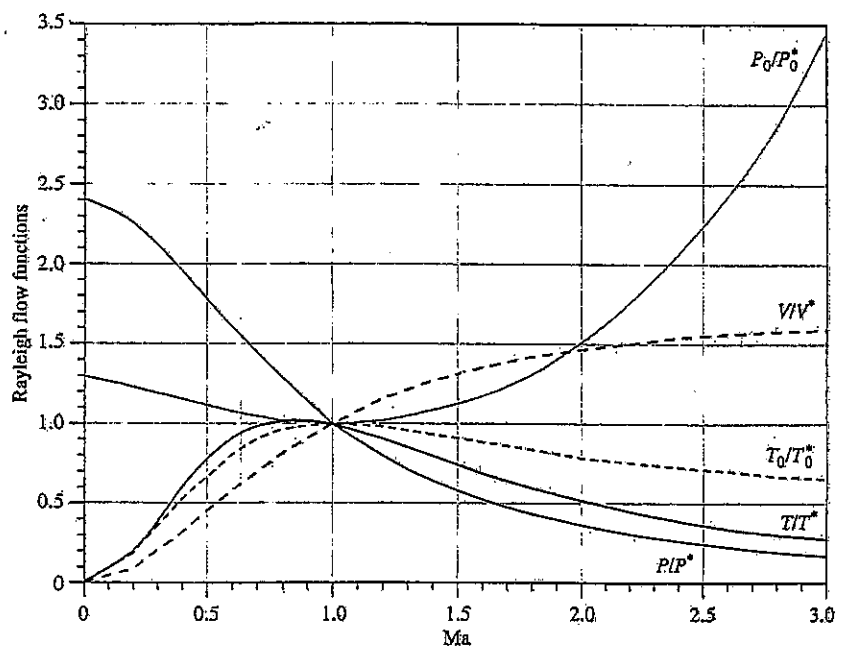
$$\frac{P}{P^*} = \frac{1+k}{1 + kMa^2}$$

$$\frac{V}{V^*} = \frac{\rho^*}{\rho} = \frac{(1+k)Ma^2}{1 + kMa^2}$$

TABLE A-15

Rayleigh flow functions for an ideal gas with $k = 1.4$

Ma	T_0/T_0^*	P_0/P_0^*	T/T^*	P/P^*	V/V^*
0.0	0.0000	1.2679	0.0000	2.4000	0.0000
0.1	0.0468	1.2591	0.0560	2.3669	0.0237
0.2	0.1736	1.2346	0.2066	2.2727	0.0909
0.3	0.3469	1.1985	0.4089	2.1314	0.1918
0.4	0.5290	1.1566	0.6151	1.9608	0.3137
0.5	0.6914	1.1141	0.7901	1.7778	0.4444
0.6	0.8189	1.0753	0.9167	1.5957	0.5745
0.7	0.9085	1.0431	0.9929	1.4235	0.6975
0.8	0.9639	1.0193	1.0255	1.2658	0.8101
0.9	0.9921	1.0049	1.0245	1.1246	0.9110
1.0	1.0000	1.0000	1.0000	1.0000	1.0000
1.2	0.9787	1.0194	0.9118	0.7958	1.1459
1.4	0.9343	1.0777	0.8054	0.6410	1.2564
1.6	0.8842	1.1756	0.7017	0.5236	1.3403
1.8	0.8363	1.3159	0.6089	0.4335	1.4046
2.0	0.7934	1.5031	0.5289	0.3636	1.4545
2.2	0.7561	1.7434	0.4611	0.3086	1.4938
2.4	0.7242	2.0451	0.4038	0.2648	1.5252
2.6	0.6970	2.4177	0.3556	0.2294	1.5505
2.8	0.6738	2.8731	0.3149	0.2004	1.5711
3.0	0.6540	3.4245	0.2803	0.1765	1.5882



Continued ...

$$T_0 = T_0^*$$

$$\frac{P_0}{P_0^*} = \frac{\rho_0}{\rho_0^*} = \frac{1}{\text{Ma}} \left(\frac{2 + (k-1)\text{Ma}^2}{k+1} \right)^{(k+1)/2(k-1)}$$

$$\frac{T}{T^*} = \frac{k+1}{2 + (k-1)\text{Ma}^2}$$

$$\frac{P}{P^*} = \frac{1}{\text{Ma}} \left(\frac{k+1}{2 + (k-1)\text{Ma}^2} \right)^{1/2}$$

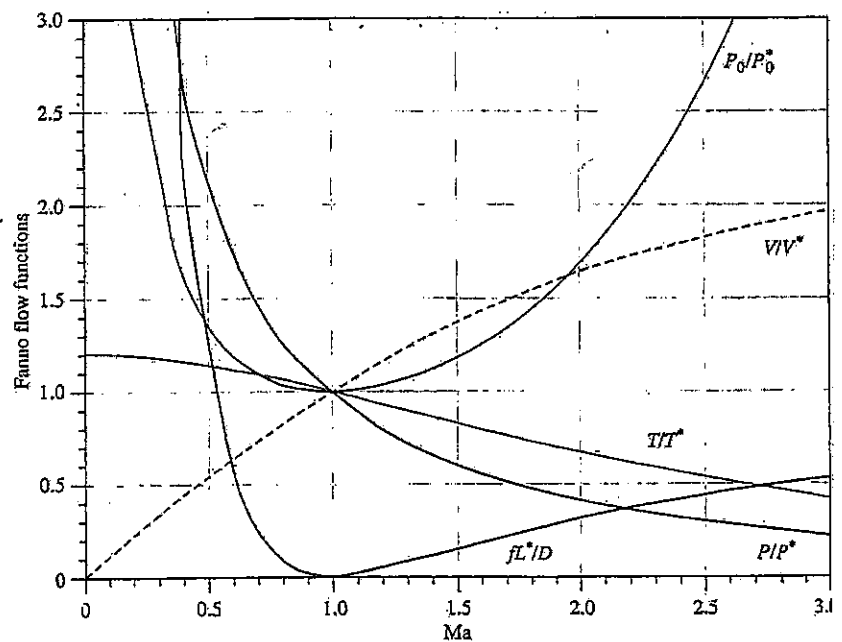
$$\frac{V}{V^*} = \frac{\rho^*}{\rho} = \text{Ma} \left(\frac{k+1}{2 + (k-1)\text{Ma}^2} \right)^{1/2}$$

$$\frac{fL^*}{D} = \frac{1 - \text{Ma}^2}{k\text{Ma}^2} + \frac{k+1}{2k} \ln \frac{(k+1)\text{Ma}^2}{2 + (k-1)\text{Ma}^2}$$

TABLE A-16

Fanno flow functions for an ideal gas with $k = 1.4$

Ma	P_0/P_0^*	T/T^*	P/P^*	V/V^*	fL^*/D
0.0	∞	1.2000	∞	0.0000	∞
0.1	5.8218	1.1976	10.9435	0.1094	66.9216
0.2	2.9635	1.1905	5.4554	0.2182	14.5333
0.3	2.0351	1.1788	3.6191	0.3257	5.2993
0.4	1.5901	1.1628	2.6958	0.4313	2.3085
0.5	1.3398	1.1429	2.1381	0.5345	1.0691
0.6	1.1882	1.1194	1.7634	0.6348	0.4908
0.7	1.0944	1.0929	1.4935	0.7318	0.2081
0.8	1.0382	1.0638	1.2893	0.8251	0.0723
0.9	1.0089	1.0327	1.1291	0.9146	0.0145
1.0	1.0000	1.0000	1.0000	1.0000	0.0000
1.2	1.0304	0.9317	0.8044	1.1583	0.0336
1.4	1.1149	0.8621	0.6632	1.2999	0.0997
1.6	1.2502	0.7937	0.5568	1.4254	0.1724
1.8	1.4390	0.7282	0.4741	1.5360	0.2419
2.0	1.6875	0.6667	0.4082	1.6330	0.3050
2.2	2.0050	0.6098	0.3549	1.7179	0.3609
2.4	2.4031	0.5576	0.3111	1.7922	0.4099
2.6	2.8960	0.5102	0.2747	1.8571	0.4526
2.8	3.5001	0.4673	0.2441	1.9140	0.4898
3.0	4.2346	0.4286	0.2182	1.9640	0.5222



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